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## Phosphorus, Sulfur, and Silicon and the Related Elements

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### Synthesis of Hydrotalcite from Seawater and Its Application to Phosphorus Removal

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## SYNTHESIS OF HYDROTALCITE FROM SEAWATER AND ITS APPLICATION TO PHOSPHORUS REMOVAL

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10.0 wt% milk of lime was added to seawater containing  $\text{AlCl}_3$  at  $\text{Mg}/\text{Al}$  molar ratio of 3.0 until pH 10.5 with stirring, and kept at 25°C for 1 h. Hydrotalcite (HT) was precipitated as a single phase, and  $\text{Mg}^{2+}$  and  $\text{Al}^{3+}$  were quantitatively precipitated. The chemical composition was  $[\text{Mg}_{0.75}\text{Al}_{0.25}(\text{OH})_2](\text{SO}_4)_{0.06}(\text{Cl})_{0.02}(\text{OH})_{0.11} \cdot 0.27\text{H}_2\text{O}$  (\*Balance). A 100 mg-P/L  $\text{Na}_2\text{HPO}_4$  solution and the HT were shaken at 25°C. Phosphate removal increased with increasing time and the HT quantity, and was the highest at pH 7–9. Phosphate ion could be quantitatively removed, adding 8 times the stoichiometric quantity of the HT at pH 8.7 for 6 h.

**Keywords:** Anion exchange; hydrotalcite; milk of lime; phosphorus removal; seawater; synthesis

## INTRODUCTION

In order to prevent eutrophication, it is considered to reduce the load of phosphorus to water environment. One method is the removal of phosphate ion by HT ( $[\text{Mg}^{2+}_{1-x}\text{Al}^{3+}_x(\text{OH})_2](\text{A}^{n-})_{x/n} \cdot m\text{H}_2\text{O}$ ;  $0.20 \leq x \leq 0.33$ ), which is a layered double hydroxide with anion exchange property;<sup>1,2</sup> however, HT is an expensive material used as antacid, etc.,<sup>3</sup> and it is necessary to develop new process for inexpensive HT. In this study, HT was synthesized using seawater and milk of lime in consideration for the utilization of plant-producing  $\text{Mg}(\text{OH})_2$ , and the characteristic of phosphate removal by the HT was examined.

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**TABLE I** The Compositions of Seawaters (mM)

Seawater	Na <sup>+</sup>	K <sup>+</sup>	Mg <sup>2+</sup>	Ca <sup>2+</sup>	SO <sub>4</sub> <sup>2-</sup>	Cl <sup>-</sup>	Br <sup>-</sup>
Artificial	466	0	53	10	28	536	0
Natural	424	9	48	11	25	500	1

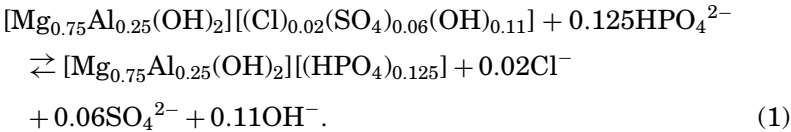
**EXPERIMENTAL**

**1. Synthesis of HT from Seawater (Seawater-Milk of Lime Process)**

Table I shows the compositions of seawaters. 0.7–10.0 wt% Ca(OH)<sub>2</sub> slurry or Ca(OH)<sub>2</sub> powder were added to artificial or natural seawater containing AlCl<sub>3</sub> at Mg/Al molar ratio of 1.0–5.0 until pH 10.5 or stoichiometric amounts with stirring and kept at 25°C or 60°C for 1 h. Precipitates were filtered, washed with water, dried at 105°C for 24 h, and then identified by X-ray diffraction (XRD). Chemical composition of filtrates and precipitates was determined by ICP-AES and ion chromatography.

**2. The Application of HT Prepared with the New Process to Phosphorus Removal**

The [Mg<sub>0.75</sub>Al<sub>0.25</sub>(OH)<sub>2</sub>][(SO<sub>4</sub>)<sub>0.06</sub>(Cl)<sub>0.02</sub>(OH)<sub>0.11</sub>]<sup>\*</sup> · 0.27H<sub>2</sub>O<sup>\*</sup> (HT<sub>(SW)</sub>) was applied to phosphorus removal. HT<sub>(SW)</sub> of 1–8 times the stoichiometric quantity were added to a 100 mg-P/L Na<sub>2</sub>HPO<sub>4</sub> solution (15 ml) according to eq. (1) at pH 7.1–13.3, and they were shaken at 25°C for 6 h:



After the filtration, chemical composition of filtrates was determined by ion chromatography.

**RESULTS AND DISCUSSION**

**1. Synthesis of HT from Seawater (Seawater-Milk of Lime Process)**

**1-1. The Effect of Mg/Al Molar Ratio in Solution (Artificial Seawater, 0.7 wt% Ca(OH)<sub>2</sub> Slurry, 60°C)**

HT was precipitated as a single phase at Mg/Al molar ratio of 2.0–4.0, although a small amount of Al(OH)<sub>3</sub> was precipitated at 1.0 and

a small amount of  $\text{Mg}(\text{OH})_2$  was precipitated at 4.5–5.0. As increasing  $\text{Mg}/\text{Al}$  molar ratio in solution,  $\text{Al}^{3+}$  precipitated increased and  $\text{Mg}^{2+}$  precipitated decreased.  $\text{Mg}^{2+}$  and  $\text{Al}^{3+}$  were quantitatively precipitated at 2.4–3.0.

### **1-2. The Effect of $\text{Ca}(\text{OH})_2$ Slurry Concentration (Artificial Seawater, $\text{Mg}/\text{Al}$ Molar Ratio of 3.0 in Solution, 25°C)**

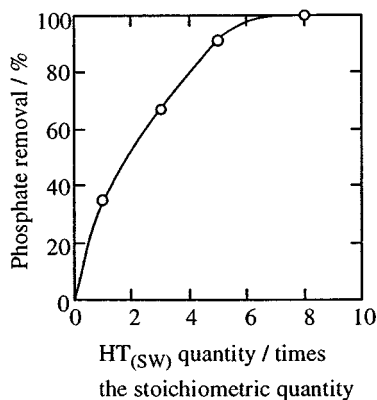
HT was precipitated as a single phase using 0.7–10.0 wt%  $\text{Ca}(\text{OH})_2$  slurry and even  $\text{Ca}(\text{OH})_2$  powder.  $\text{Mg}^{2+}$  and  $\text{Al}^{3+}$  were quantitatively precipitated.

### **1-3. Synthesis of HT from Natural Seawater ( $\text{Mg}/\text{Al}$ Molar Ratio of 3.0 in Solution, 10.0 wt% $\text{Ca}(\text{OH})_2$ Slurry, 25°C)**

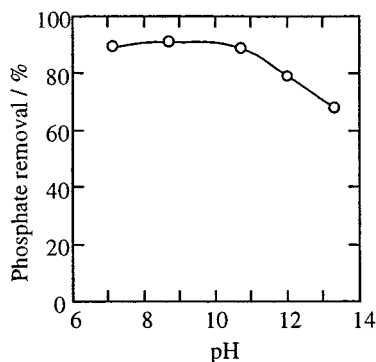
HT ( $\text{HT}_{(\text{SW})}$ ) was also precipitated as a single phase from natural seawater, as well as from artificial seawater, and  $\text{Mg}^{2+}$  and  $\text{Al}^{3+}$  were quantitatively precipitated. The chemical composition of  $\text{HT}_{(\text{SW})}$  was  $[\text{Mg}_{0.75}\text{Al}_{0.25}(\text{OH})_2][(\text{SO}_4)_{0.06}(\text{Cl})_{0.02}(\text{OH})_{0.11}] \cdot 0.27\text{H}_2\text{O}^*$  (\*Balance). The ratio of  $\text{SO}_4^{2-}$  to  $\text{Cl}^-$  in the interlayer was high. This is because the charge density of  $\text{SO}_4^{2-}$  is larger than that of  $\text{Cl}^-$ . Anion is easily intercalated into HT, as the charge density is larger.<sup>4</sup>

## **2. The Application of HT Prepared with the New Process to Phosphorus Removal**

Figure 1 shows the effect of  $\text{HT}_{(\text{SW})}$  quantity on phosphate removal. Phosphate removal increased with increasing the  $\text{HT}_{(\text{SW})}$  quantity, and



**FIGURE 1** Effect of  $\text{HT}_{(\text{SW})}$  quantity on phosphate removal (pH 8.7).



**FIGURE 2** Effect of pH on phosphate removal using  $\text{HT}_{(\text{SW})}$  of 5 times the stoichiometric quantity.

phosphate ion could be quantitatively removed by adding 8 times the stoichiometric quantity of  $\text{HT}_{(\text{SW})}$ ; however, phosphate ion was not quantitatively removed at the stoichiometric quantity. The ionic species of phosphate at pH 8.7 are mainly  $\text{HPO}_4^{2-}$ . Because the anion size of  $\text{HPO}_4^{2-}$  is almost close to that of  $\text{SO}_4^{2-}$ ,<sup>5</sup> it is supposed that  $\text{HPO}_4^{2-}$  was not much exchanged for  $\text{SO}_4^{2-}$  in  $\text{HT}_{(\text{SW})}$ . Figure 2 shows the effect of pH on phosphate removal. Phosphate removal was the highest at pH 7–9 and decreased with increasing pH. The ionic species of phosphate at pH 13.3 are mainly  $\text{PO}_4^{3-}$ . Although the charge density of  $\text{PO}_4^{3-}$  is larger than that of  $\text{SO}_4^{2-}$ , the phosphate removal was the lowest. Because of the large amounts of  $\text{OH}^-$  at the pH, it is supposed that  $\text{OH}^-$  was mainly intercalated into  $\text{HT}_{(\text{SW})}$ , and the intercalation of  $\text{PO}_4^{3-}$  was prevented. In contrast, although the existence ratio of  $\text{HPO}_4^{2-}$  was low since the ionic species at pH 7.1 were a mixture of  $\text{HPO}_4^{2-}$  (44%) and  $\text{H}_2\text{PO}_4^-$  (56%), the phosphate removal at pH 7.1 was almost as same as that at pH 8.7. This is attributable to the increase in the  $\text{HPO}_4^{2-}$  in solution with the deintercalation of  $\text{OH}^-$  in  $\text{HT}_{(\text{SW})}$ .

## REFERENCES

- [1] A. Kawamoto, A. Ookubo, T. Sato, and T. Suzuki, *Mizukannkyougakkaishi*, **22**, 875 (1999).
- [2] H. Shin, M. Kim, S. Nam, and H. Moon, *Water Sci. Tech.*, **34**, 161 (1996).
- [3] F. Cavani, F. Trifiro, and A. Vaccari, *Catal. Today*, **11**, 173 (1991).
- [4] S. Miyata, *Clays Clay Miner.*, **31**, 305 (1983).
- [5] T. Sato, T. Wakabayashi, and M. Shimada, *Ind. Eng. Chem., Process Des. Dev.*, **25**, 89 (1986).